

# Snel besparen op energie, kosten én CO2

**Marcel Kelder**  
Smart Manufacturing specialist

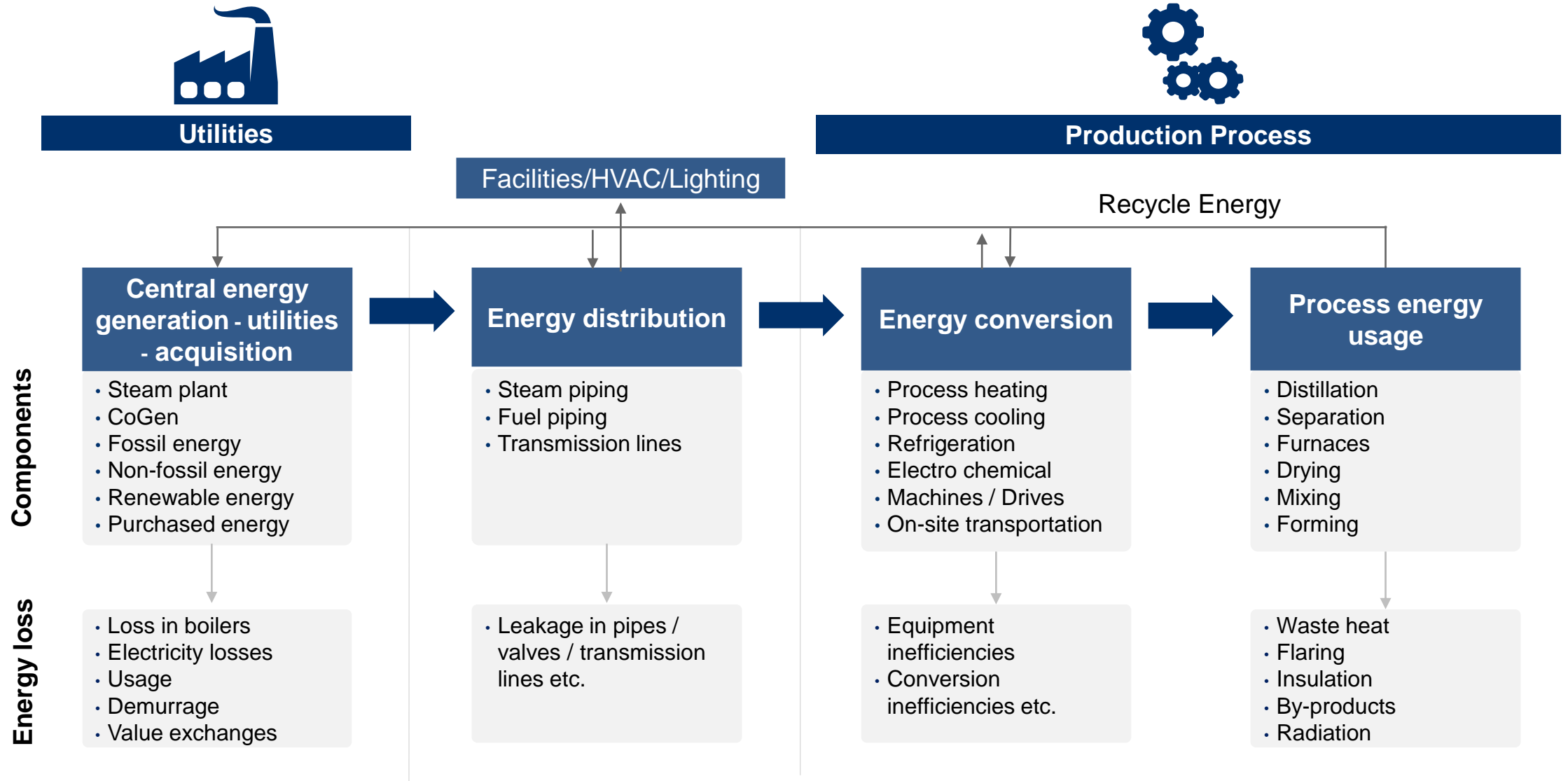
24.01.23



- Productie Proces Automatisering



# The influences of energy loss



# Return on investment



If energy costs are

**20%**

of all production costs,



and If gross profit is at

**15%**

of all production costs,



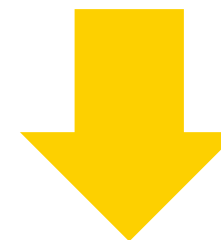
and if

**10%**

Improvement of energy performance is achieved...

## THE RESULT IS

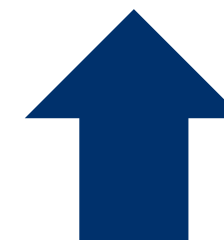
**2%**



Decrease in production costs



**13.33%**

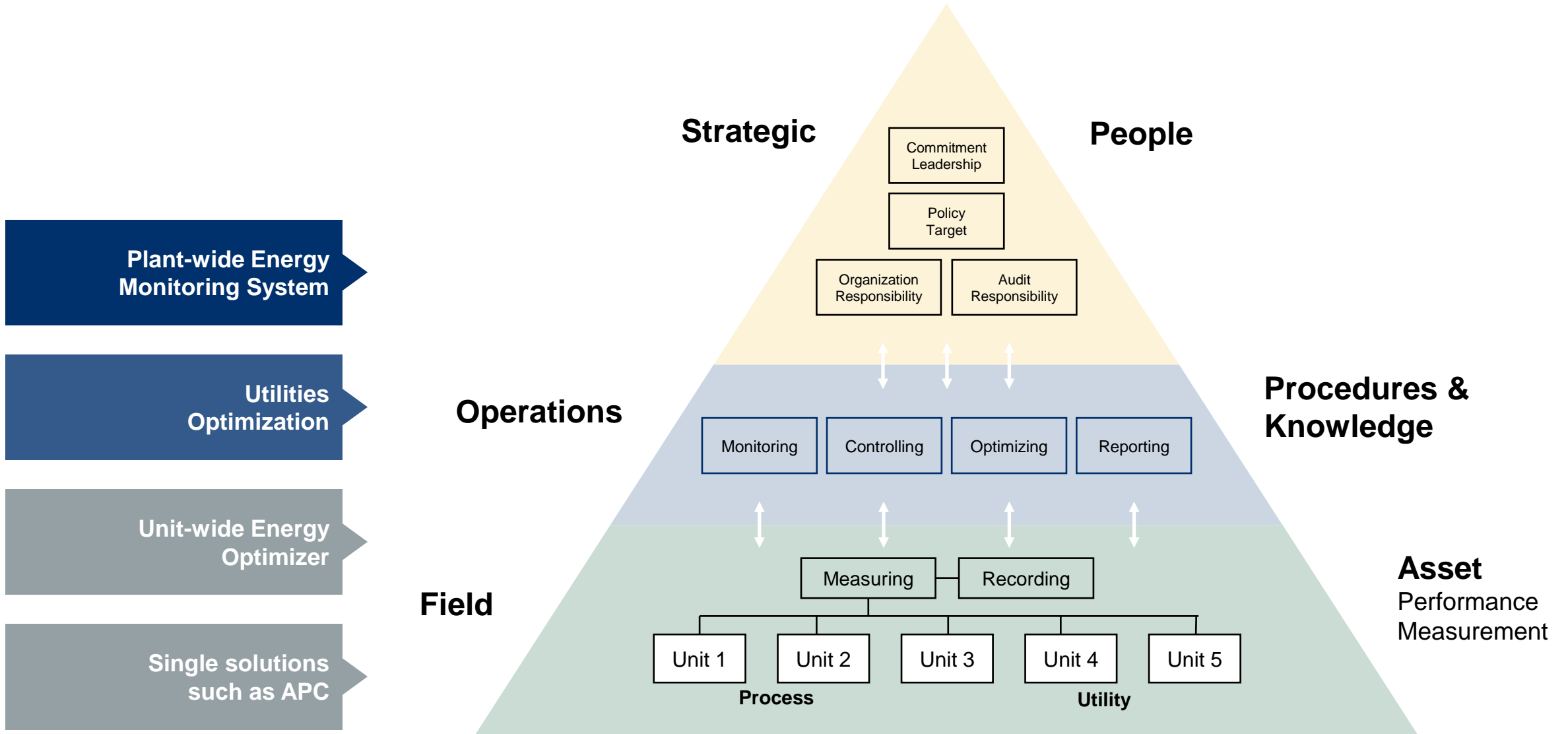


Increase in profit

(all other factors assumed to remain constant)



# Energy and environmental management structure







Utilities

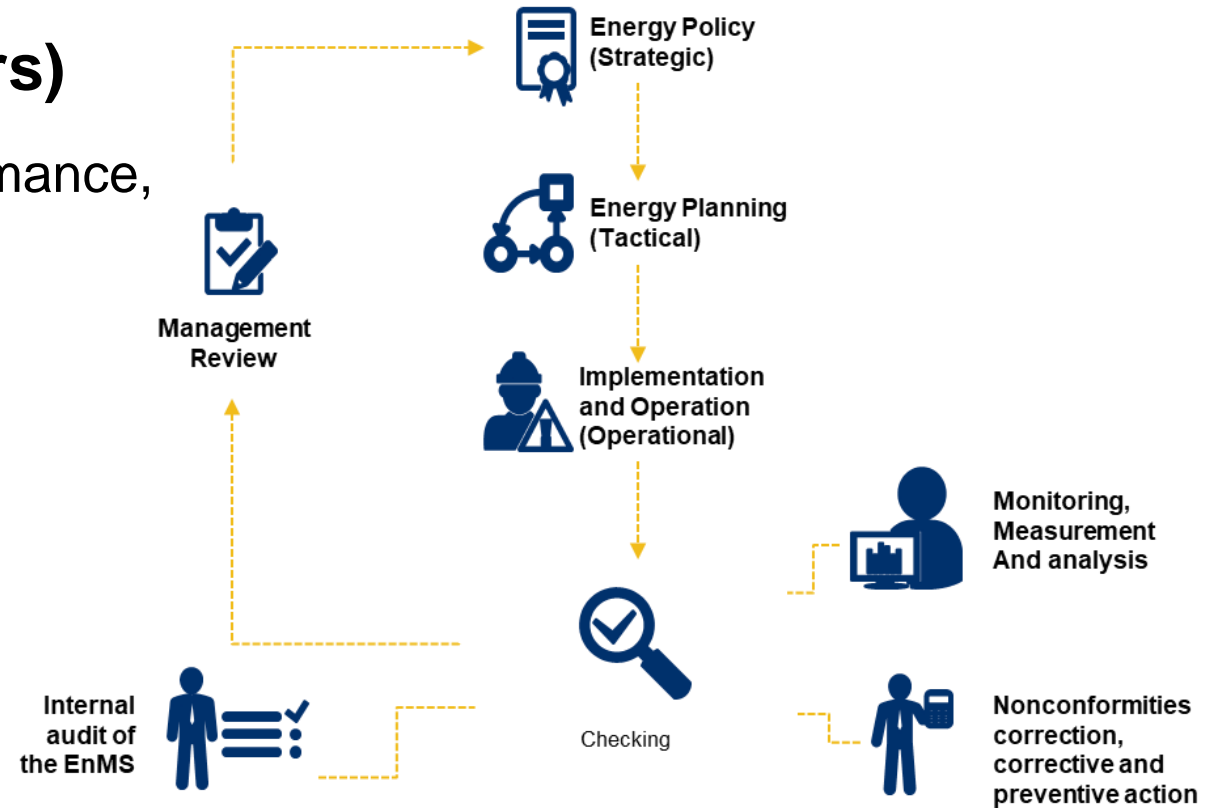
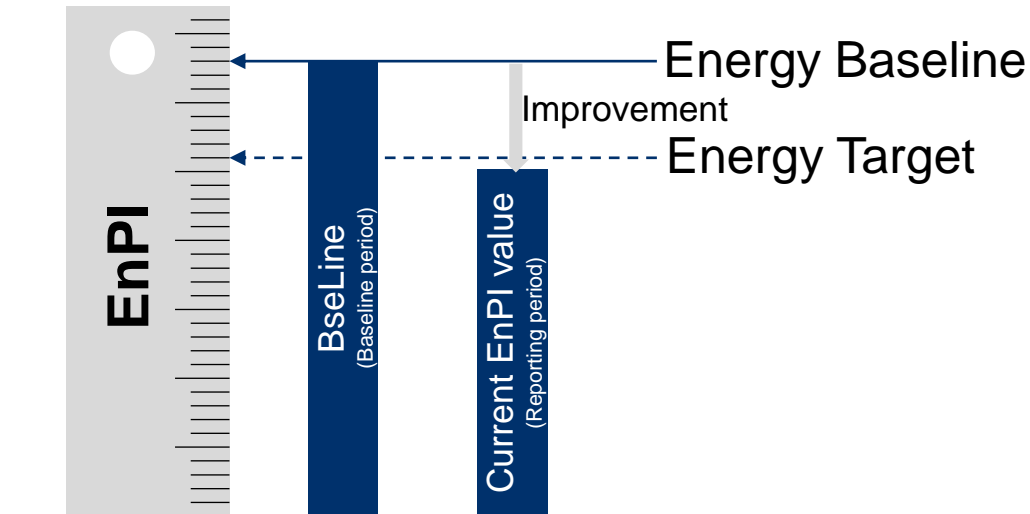
Production Process

- **EnPIs (Energy Performance Indicators)**

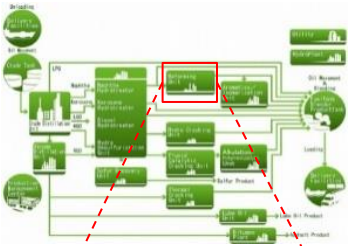
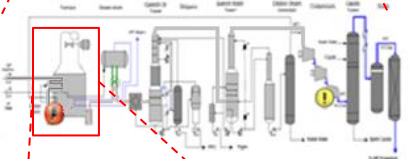
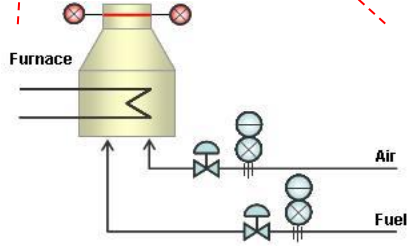
Quantitative value or measure of energy performance, as defined by the organization

- **Energy Baseline**

Quantitative reference(s) providing a basis for comparison of energy performance

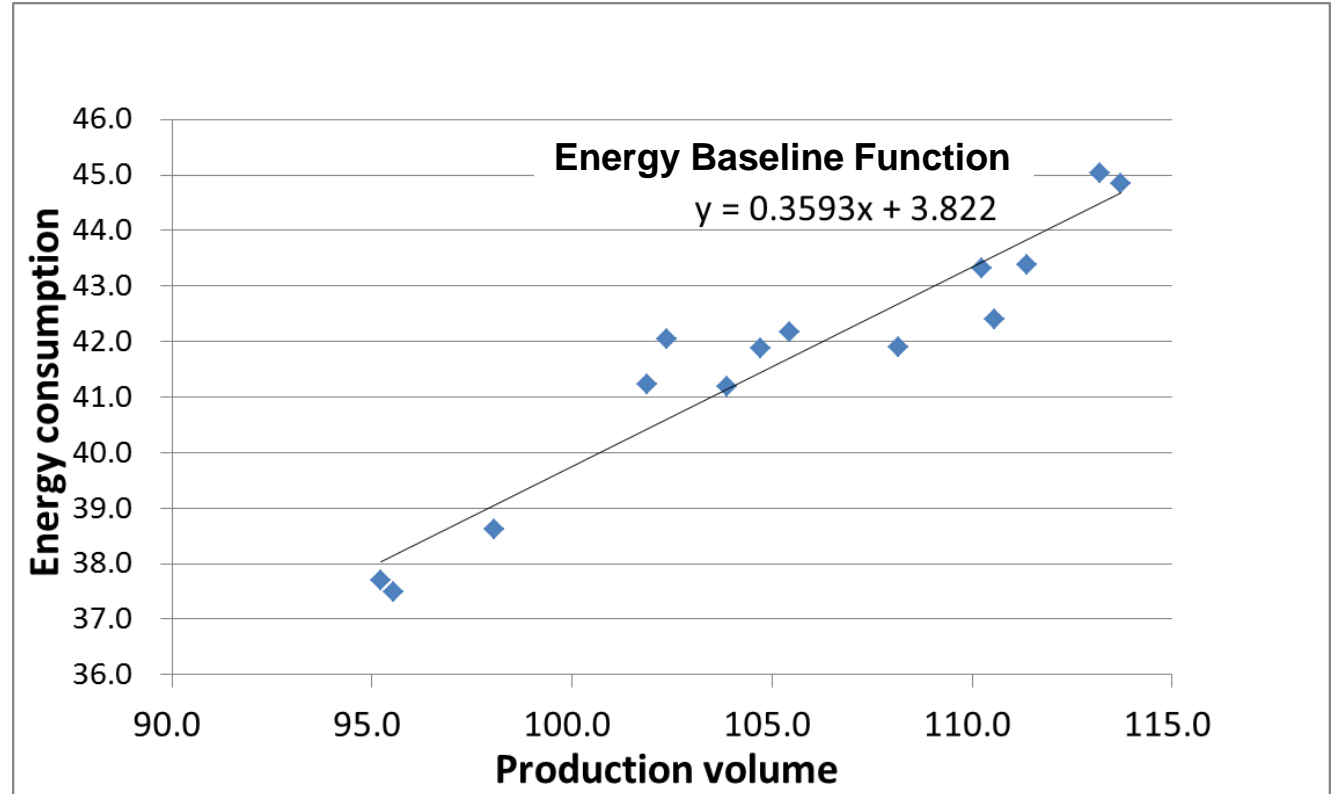




Layer	Boundary	EnPIs
Plant	Refinery 	<ul style="list-style-type: none"> <li>• Oil refinery energy intensity = (energy consumption of entire oil refinery) / (topping plant conversion throughput of the entire oil refinery)</li> <li>• The topping plant conversion throughput of the entire oil refinery = total {(CF value for every unit) *} (throughput for every unit)</li> </ul>
Unit	Reforming 	<ul style="list-style-type: none"> <li>• Energy intensity = (input energy consumption) / (the amount of feed)</li> <li>• Energy utilization efficiency</li> <li>• The rate of the heat recovery</li> <li>• Capacity usage ratio</li> </ul>
Device	Furnace 	<ul style="list-style-type: none"> <li>• Energy efficiency = (feed heating value) / (combustion heat quantity)</li> <li>• Heat conduction efficiency</li> <li>• Coil path balance</li> <li>• Air fuel ratio</li> <li>• Exhaust gas O2 concentration</li> </ul>



“Energy Baseline function is defined from historical track record of energy use and analysis with statistical method”



\* It can be done by an energy specialist







## Traditional Systems

Particular operating case



History/snapshot



Ad-hoc basis to answer a question



Owned and used by isolated groups



Specific tools for different silos



## Real-time Digital Twin

Full range of asset operation, with auto-adaptation in real-time

History, real-time and **future**

Automated to consider business workflows

Centralized single version of the truth, used by everyone

Single integrated twin for energy, utilities and related systems



## Energy Digital Twin

- Real time mass balance
- Real time energy consumption
- Real time energy efficiency
- Real time emissions
- Run if then else scenarios
- KPI reporting

## Real-time Energy Optimizer

- Real time cost calculation
- Real time cost savings
- Real time operator instructions

### Energy KPI

Energy Digital Twin /  
Mass Balance System



Energy



€ / US\$

Financial  
Balance System plus  
Optimization

Freedom to switch between  
steam and electrical and to  
switch between import and  
export

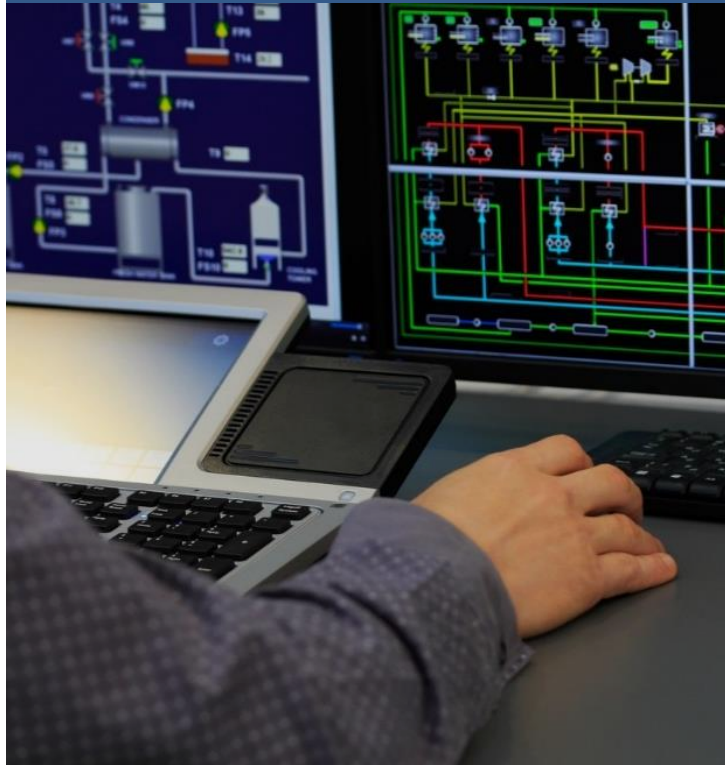


## PAST



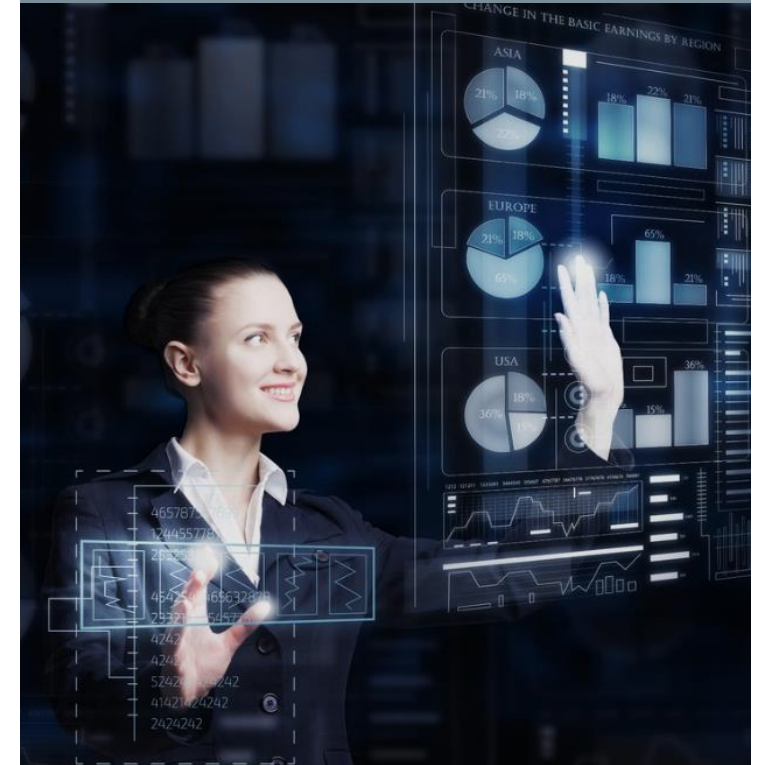
**MONITORING & REPORTING**

## PRESENT



**OPTIMIZATION**

## FUTURE



**SCHEDULING & PLANNING**



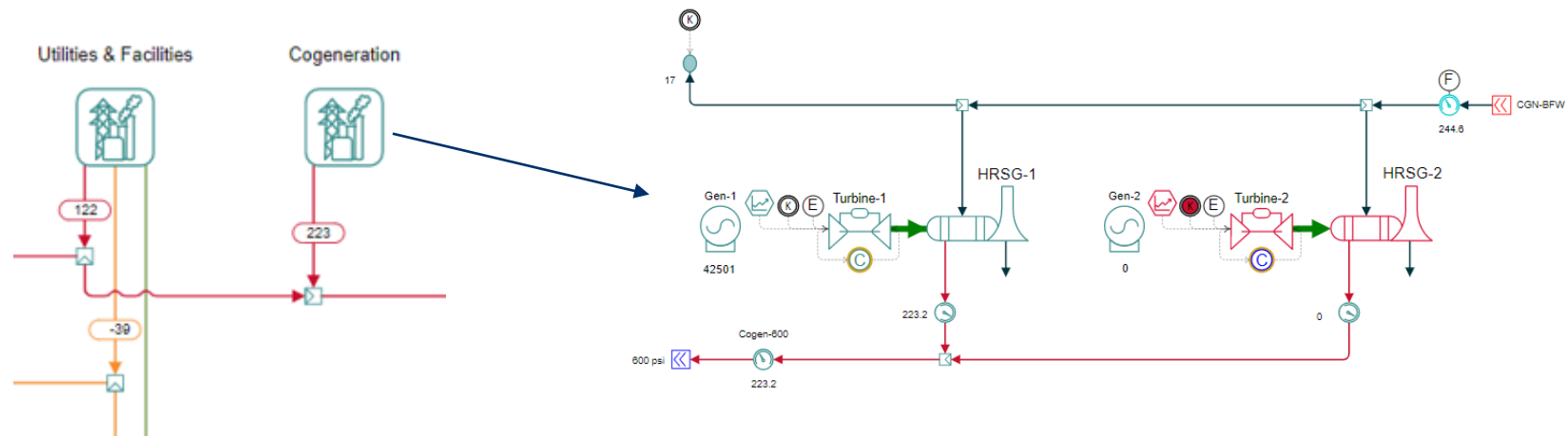


PAST



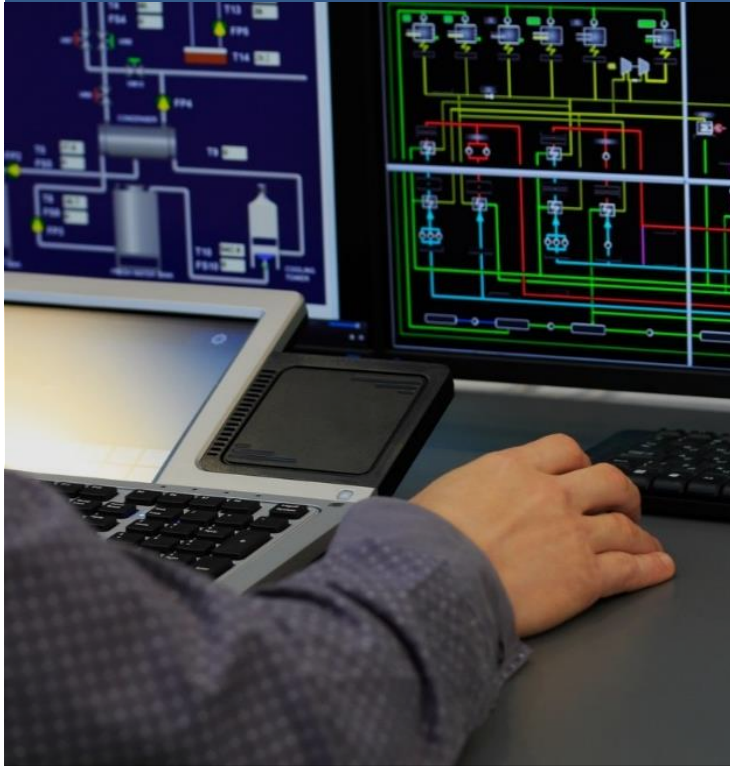
MONITORING & REPORTING

- **Accounting** and auditing of utilities
- **Emissions** management and monitoring
- Equipment **performance** monitoring
- Energy system **evaluation**
- **Corporate/site-wide visibility** to energy system



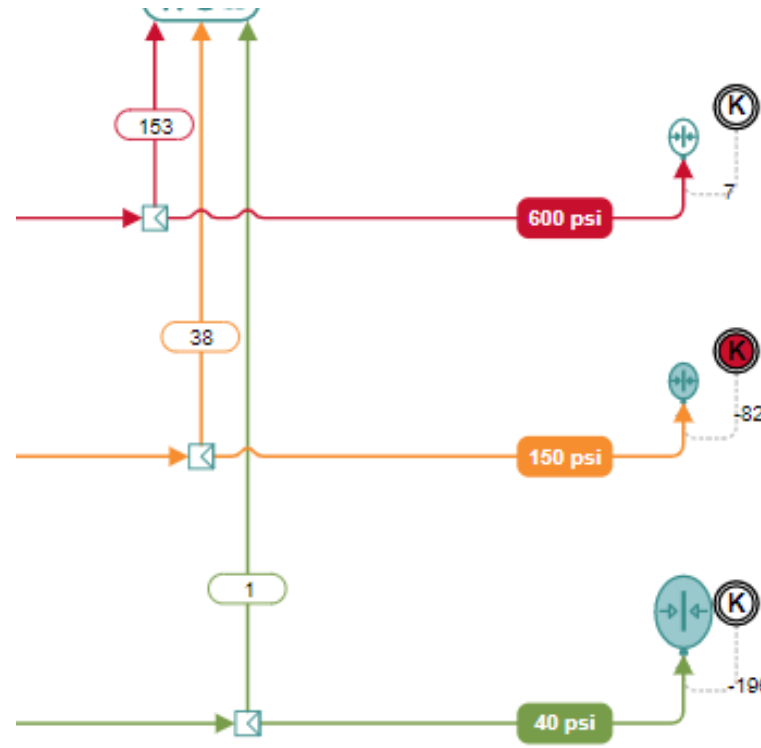


PRESENT



OPTIMIZATION

- Real-time emissions and KPIs
- Real-time imbalances
- Utilities Real Time Optimizer



	Actual	Optimized	Delta
<b>Boiler Plant</b>			
Boiler-1 FG (MSCF/HR)	100.1	31.2	-68.9 ↓
Boiler-2 Steam (KLB/HR)	106.0	61.4	-44.7 ↓
Boiler-3 FG (MSCF/HR)	72.6	69.6	-3.1 ↓

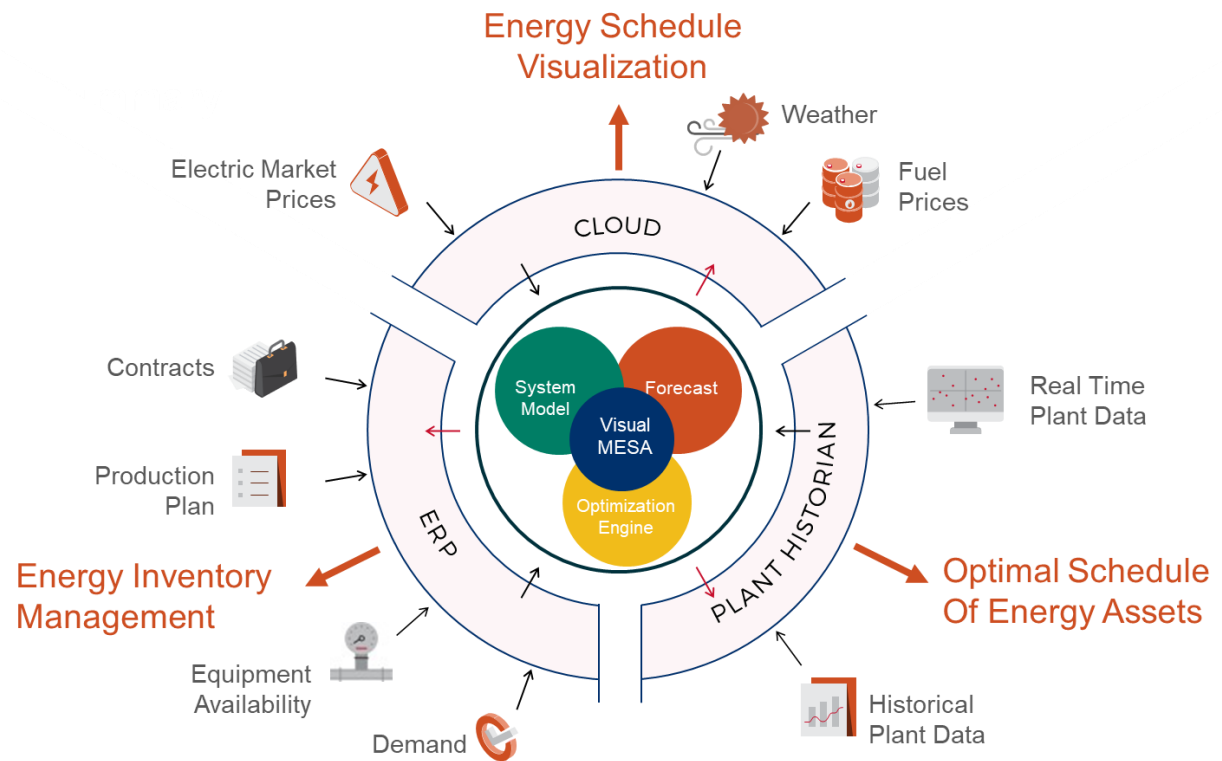
<b>GTs</b>			
Turbine-1 Electric power (MW)	41.0	42.2	1.2 ↑
HRSG-1 Steam (KLB/HR)	223.1	355.1	132.0 ↑
Turbine-2 Power (MW)	0.0	0.0	0.0 =
HRSG-2 Steam (KLB/HR)	0.0	0.0	0.0 =

<b>Re-Gasification Plant Compressors</b>			
BOG C-101 Extraction (KLB/HR)	350.4	350.4	0.0 =
C-102 Extraction (KLB/HR)	85.1	108.5	23.4 ↑

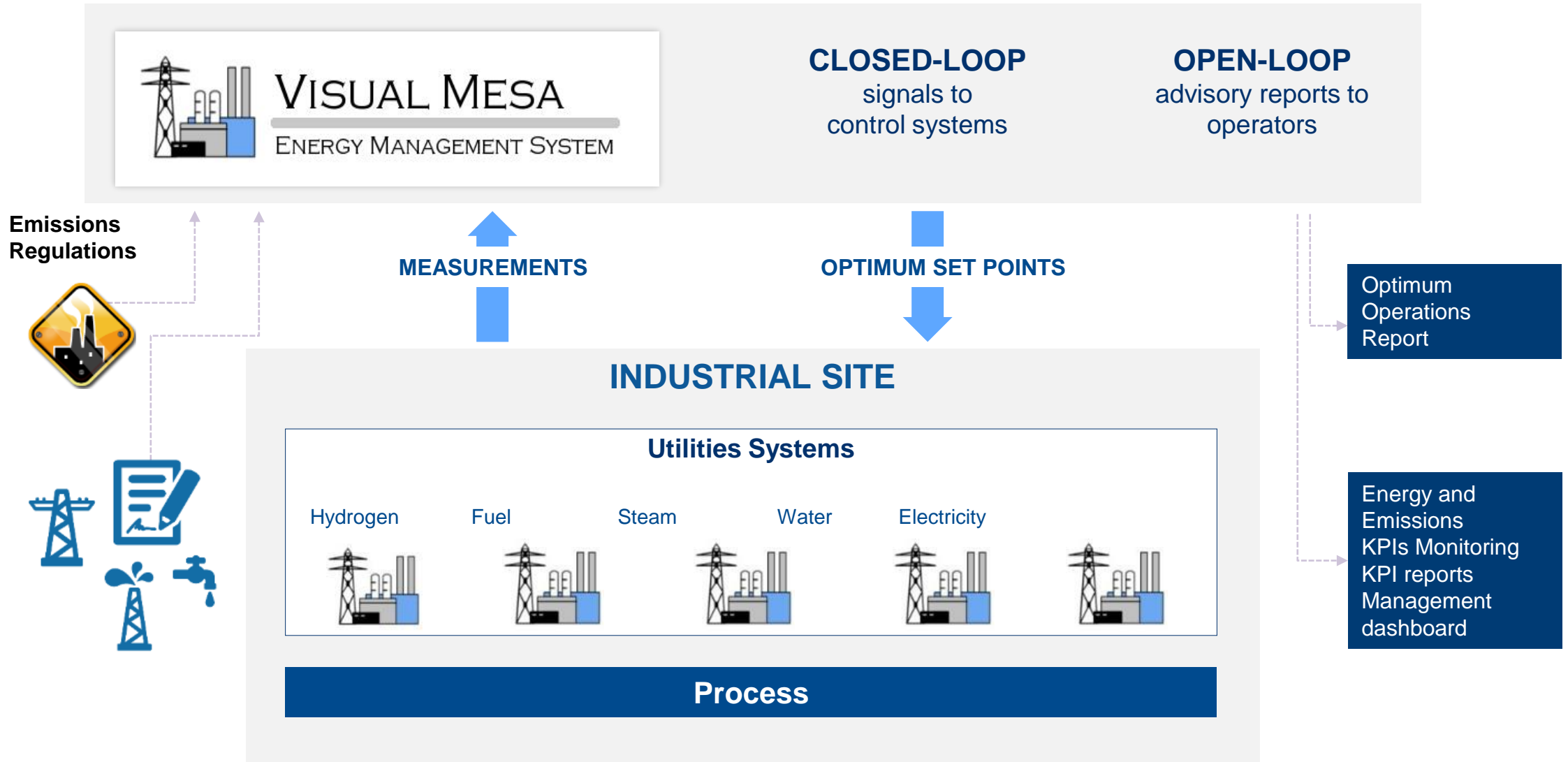
Turbines and Motors Swaps		Total T/M Swaps: 4	
Unit	Driver	Actual Status	Optimized Status
CRUDE	TP-5103	Stopped	Running
CRUDE	MP-5103A	Running	Stopped
CRUDE	TP-5155A	Running	Stopped
CRUDE	MP-5155	Stopped	Running
CT-PUMPS	TP-104	Stopped	Running
CT-PUMPS	MP-104	Running	Stopped
6-CT	6P-1	Stopped	Running
6-CT	6P-4	Running	Stopped



- Investment planning and **basic engineering**
- Support of decision making in complex environment



# Energy real time optimizer (ERTO)



- Imbalances
- Efficiencies
- Consumptions
- Emissions
- Sensor validation
- Cost calculation
- Alarms
- Reporting

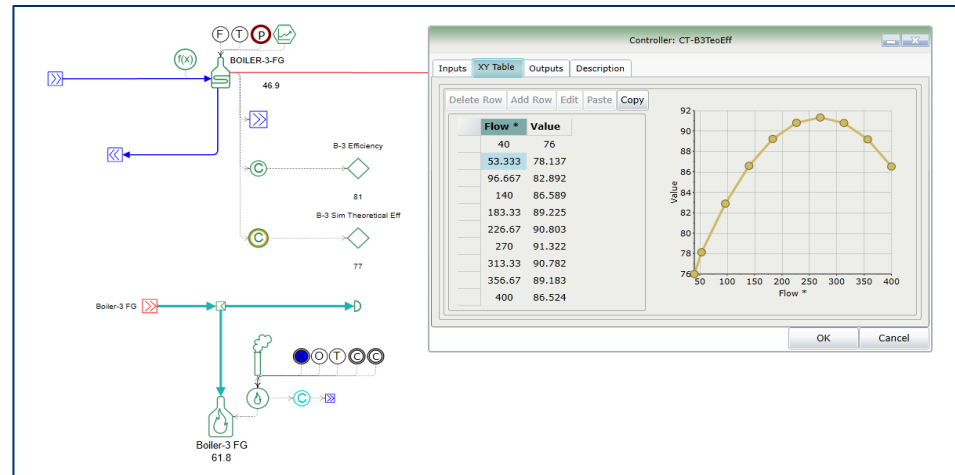
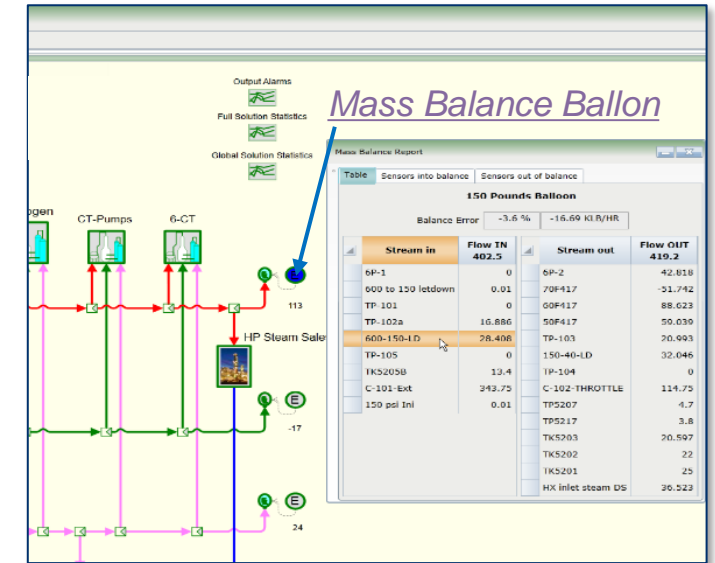
Process Plant Cost: PPC-CRUDE

Inputs Plant Cost Description

Stream Costs

Stream	Block Name	Flow	Units	Unit Cost (\$ per unit flow)	Cost \$ per hour	Energy	Units	Equiva Hea (mmB/HR)
Total: (7 items)								
600 psi	60F416	10.5997799	KLB/HR	4.0481	42.91	13.81925	mmBTU/HR	13.815
150 psi	60F417	80.9799111	KLB/HR	3.6894	298.77	99.24677	mmBTU/HR	99.246
40 psi	60F418	22.9130559	KLB/HR	2.2736	52.09	27.30591	mmBTU/HR	27.305
Water	CRUDE BFW	71.5990786	KLB/HR	0.5982	42.83	18.72962	mmBTU/HR	18.729
Electricity	Crude Power	3429.568	KW	0.0802	275.05	3429.568	KW	34.295
Fuel Oil	FO to Furnace	64.4471432	mmBTU/HR	6.0000	386.68	64.44714	mmBTU/HR	64.447
Refinery Gas	FG to Furnace	86.6605786	mmBTU/HR	3.0938	268.11	86.66058	mmBTU/HR	86.660

Plant Feed or Production Rate: 4.2037296    Total Energy In: 344.50496  
 Energy per Unit Plant Rate: 74.451553    Total Energy Out: 31.53076



Inputs Flue Gas Properties Emissions Components Description

Simulation

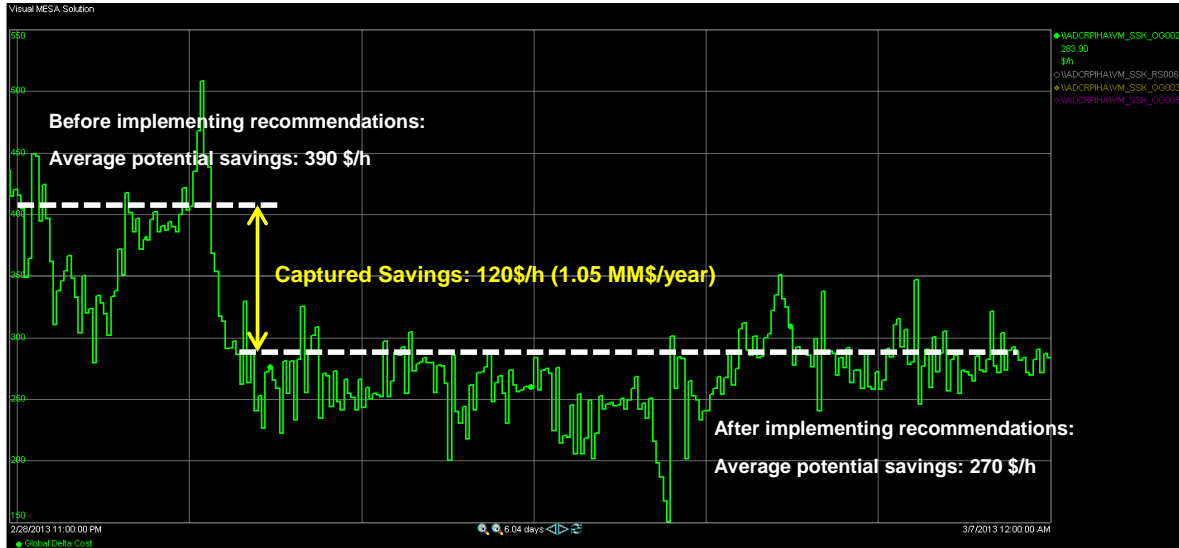
	Mass (KLB/HR)	Mass/Duty (KLB/MMBTU)	Mass/Volume (KLB/MSCF)	Concentration (mass %)	Concentration (vol %)
Carbon Dioxide	9.936	0.1132	0.009191	12.48	7.884
Sulfur Dioxide	0.3344	0.003808	0.0003093	0.42	0.186
Nitrogen Oxide	0.01756	0.0002	1.625E-05	0.02206	0.000194

Global

	Mass (KLB/HR)	Mass/Duty (KLB/MMBTU)	Mass/Volume (KLB/MSCF)	Concentration (mass %)	Concentration (vol %)
Carbon Dioxide	3.27	0.1132	0.009194	12.48	7.887
Sulfur Dioxide	0.1062	0.003678	0.0002986	0.4055	0.1796
Nitrogen Oxide	0.005775	0.0002	1.624E-05	0.02205	0.0001939







Around 3:00 AM on March 2<sup>nd</sup>, Operators applied one of the optimization actions calculated by the RTEMS and 1.05 MM\$/year of savings were immediately captured (i.e., the predicted savings trend drops)

Extraction-Condensing Turbines in the Olefins plant (t/h)

KT-13001 VHP Steam Inlet	171	362	191	Manual Action
KT-13001 HP Steam Extraction	0	243	243	
KT-13001 Outlet Condensate	121	69	-52	
KT-15010 VHP Steam Inlet	194	315	121	Manual Action
KT-15010 MP Steam Extraction	46	260	214	
KT-15010 Outlet Condensate	142	48	-94	
KT-15020 HP Steam Inlet	211	240	29	Manual Action
KT-15020 LP Steam Extraction	46	106	60	
KT-15020 Outlet Condensate	141	111	-30	

Turbines and Motors Swaps

Total TM Swaps: 2

Area	Unit	Driver	Name	Power (HP)	Steam Levels	Action to be taken
U&O	711	Turbine	BO-71102D-BLT01	885	HP to MP	Turn Turbine OFF
U&O	711	Motor	BO-71102D-BLM01	885		Turn Motor ON
U&O	722	Turbine	PT-72201B	3500	HP to LP	Turn Turbine ON
U&O	722	Motor	PM-72201E	3500		Turn Motor OFF

Visual MESA Recommendations Report is available to everyone through the Web Browser

## Co-innovating tomorrow™

Bedankt voor uw aandacht!

Meer info:

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